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Wastewater Feasibility Study

# WASTEWATER FEASIBILITY STUDY

# CAYMUS VINEYARDS

Rurtherford, California APN 030-200-066



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# LIST OF ENCLOSURES

Enclosure A: Overall Site Plan (UP1), Wastewater Treatment Plan (UP4), Concept Wastewater Utility Plan

(UP5), Existing Wastewater Treatment (UP8)

Enclosure B: PW Pond/Effluent Dispersal Water Balance (Phase II)

Project No. 2013044

#### PROJECT OVERVIEW

Caymus Vineyards is applying for a Use Permit Modification for the existing winery facility located in Rutherford, Napa County, California with a Phase I production capacity of 110,000 gallons and a Phase II maximum capacity of 660,000 gallons. The existing Lyve System (process wastewater) and existing leachfield (sanitary sewage) will be used for Phase I. A combined process wastewater (PW) and sanitary sewage (SS) system (improved Lyve System) will be used for Phase II. An overview of this management system is discussed in this report.

#### SITE DESCRIPTION

The property is located at the intersection of Rutherford and Conn Creek Roads, east of the town of Rutherford with Conn Creek running along the eastern edge of the winery facility and through the middle of the parcel. The parcel is relatively flat except for the banks of Conn Creek.

The existing winery facility includes an assortment of buildings (some of which will be demolished and rebuilt). An existing irrigation pond and vineyards are located to the east of Conn Creek.

#### WASTEWATER MANAGEMENT SYSTEM

PW and SS will initially continue to be plumbed and treated separately in their respective, existing systems. For Phase II, PW and SS will initially continue to be plumbed separately and will then be combined at the existing Lyve System which will remain in Building B3. Effluent will be sent from Lyve System, through a 2" forcemain (utilizing an existing 2" pipeline that crosses Conn Creek) out to the existing irrigation pond, which is proposed to be converted to an effluent storage pond. From the effluent storage pond, effluent will be utilized for onsite surface irrigation disposal.

This section of the wastewater feasibility study details the PW and SS characteristics and proposed wastewater management system.

# PROCESS WASTEWATER CHARACTERISTICS

PW will consist primarily of wastewater collected at floor drains and trenches within the winery, receiving, crush, tank, and washdown areas. Any exterior tank and process areas not under a roof will be provided with automated diversion capability to provide a means of routing rainwater to the storm drainage system when those areas are not in use for process purposes. No distillation will occur at the facility; hence there will be no stillage waste. Typical winery wastewater characteristics are as summarized below:

Characteristic	<u>Units</u>	Crushing Season Range	Non-crushing Season Range
рН		2.5 - 9.5	3.5 - 11.0
Dissolved Oxygen	mg/L	0.5 - 8.5	1.0 - 10.0
BOD₅	mg/L	500 – 12,000	300 – 3,500
COD	mg/L	800 - 15,000	500 – 6,000
Grease	mg/L	5 - 30	5 - 50
Settleable Solids	mg/L	25 - 100	2 - 100
Nonfilterable Residue	mg/L	40 - 800	10 - 400
Volatile Suspended Solids	mg/L	150 - 700	80 - 350
<b>Total Dissolved Solids</b>	mg/L	80 – 2,900	80 – 2,900
Nitrogen	mg/L	1 - 40	1 - 40
Nitrate	mg/L	0.5 - 4.8	.5
Phosphorous	mg/L	1 - 10	1 - 40
Sodium	mg/L	35 - 200	35 - 200
Alkalinity (CaCO <sub>3</sub> )	mg/L	40 - 730	10 - 730
Chloride	mg/L	3 - 250	3 - 250
Sulfate	mg/L	10 - 75	20 - 75

# SANITARY SEWAGE CHARACTERISTICS

Sanitary sewage (SS) will consist primarily of wastewater generated from restrooms, laboratory, employee kitchen, and tasting room facilities. Typical sanitary sewage characteristics are as summarized below:

Characteristic	<u>Units</u>	Raw Wastewater <sup>1</sup> Range
BOD <sub>s</sub>	mg/L	110 - 220
Grease	mg/L	50-100
Total Suspended Solids (TSS)	mg/L	100 - 220
Volatile Suspended Solids	mg/L	80 - 165
Total Dissolved Solids (TDS)	mg/L	250 - 500
Nitrogen	mg/L	20 - 40
Nitrate	mg/L	0
Phosphorous	mg/L	4 - 8
Alkalinity (CaCO <sub>3</sub> )	mg/L	50 - 100
Chloride	mg/L	30 - 50
Sulfate	mg/L	20 - 30

<sup>&</sup>lt;sup>1</sup>Typical composition of untreated domestic wastewater, Metcalf & Eddy, "Wastewater Engineering, Third Edition", 1991

#### PROCESS WASTEWATER DESIGN FLOWS (PHASE I)

Based on typical flow data from wineries of similar size and characteristics and corresponding PW generation rates, projected flows are calculated as follows:

#### **Annual Volume**

Annual production (projected)

= 110,000 gal wine/year

PW generation rate (assumed)

4 gal PW/gal wine

=

PW flow

110,000 gal wine x 4 gal PW/gal wine

= 440,000 gal PW/year

Average Day Flow

440,000 gal PW/365 days

1,210 gal PW/day

#### Average Day, Peak Month Flow

The harvest month of September accounts for approximately 16.4 percent of the annual PW flow.

440,000 gal PW x (0.164)

2,400 gal PW/day

30 day Napa County Peak Day

110,000 gallons wine x 1.5

2,750 gal PW/day

60 day harvest

The peak PW flow rate for Phase I is expected to be 2,750 gal/day.

All PW generated from Phase I will continue to be treated in the existing Lyve System. As approved in the existing Very Minor Modification (#P08-00519-VMM), hold and haul will be utilized for the disposal of treated PW from the Lyve System.

#### SANITARY SEWAGE (PHASE I)

Sanitary sewage generated from the existing approved activities will continue to be disposed of in the existing leachfield system. No change in SS flows are proposed. Therefore, no changes are proposed to the existing system.

#### PROCESS WASTEWATER DESIGN FLOWS (PHASE II)

#### **Annual Volume**

Annual production (projected) = 660,000 gal wine/year PW generation rate (assumed) = 4 gal PW/gal wine

PW flow = 660,000 gal wine x 4 gal PW/gal wine

2,640,000 gal PW/year

**Average Day Flow** 

2,640,000 gal PW/365 days = 7,240 gal PW/day

Average Day, Peak Month Flow

The harvest month of September accounts for approximately 16.4 percent of the annual PW flow.

2,640,000 gal PW x <u>(0.164)</u> = <u>14,400 gal PW/day</u> 30 day

Napa County Peak Day

660,000 gallons wine x 1.5 = 16,500 gal PW/day 60 day harvest

The peak PW flow rate for Phase II is expected to be 16,500 gal/day.

#### SANITARY SEWAGE DESIGN FLOWS (PHASE II)

The proposed winery SS flows for Phase II at Caymus will consist of typical wastewater generated from restrooms, laboratory, and employee kitchen facilities. The anticipated peak winery SS flow is summarized below:

Peak Tasting Day w/o Event							
Employee (full-time)	42	X	15	gpcd	=	630	gal/day
Employee (part-time)	14	×	15	gpcd	=	210	gal/day
Tasting Visitors	450	×	3	gpcd	=	1,350	gal/day
Total					=	2,190	gal/day
Peak Tasting Day w/ Event							
Employee (full-time)	42	×	15	gpcd	=	630	gal/day
Employee (part-time)	14	×	15	gpcd	$(i=1)^{n}$	210	gal/day
Tasting Visitors	450	×	3	gpcd	=	1,350	gal/day
Event Visitors	100	x	15	gpcd	=	1,500	gal/day
Total					=	3,690	gal/day

The peak SS flow rate associated with Phase II is expected to be 3,690 gal/day.

#### TOTAL WASTEWATER DESIGN FLOWS (PHASE II)

The peak flow rate from the two waste streams for Phase II is expected to be 20,190gpd (16,500 gpd of PW and 3,690 gpd of SS).

#### WASTEWATER CONVEYANCE, TREATMENT AND DISPOSAL (PHASE II)

The winery treatment and disposal system for Phase II will consist of the components described below. Refer to the wastewater management system schematic in Enclosure A for a flow diagram of the wastewater management system.

- Initial screening Provided by screened baskets and strainers installed on the trench drains and floor drains within the winery. Screen opening sizes will be approximately 1/4 inch for exterior drains and 1/8 inch for interior drains.
- Gravity collection system New gravity collection piping to serve the winery PW and SS should be designed to provide low maintenance and no infiltration or exfiltration. Piping must satisfy Uniform Plumbing Code and local requirements.
- Septic Tanks There is a series of existing septic tanks that will be continued to be used. These tanks
  will overflow SS to the existing Lyve system (a pump sump may be required).
- 4) Pump Sump PW that will following the automated stormwater diversion valve, may need to be collected in a sump and pumped to the existing Lyve system.
- Screening/Settling Tank It is proposed to utilize the existing solids screen prior to sending PW to the equalization zone/Lyve system.
- 6) Lyve System Treatment of combined wastewater will be accomplished in the existing Lyve treatment system which is a packaged treatment systems specifically oriented towards winery wastewater. Lyve utilizes aerobic activated sludge treatment in a modular design. These systems are capable of producing high quality effluent while taking up a small footprint. A custom, above grade concrete treatment tank will be utilized for the Lyve system. Internal zones are proposed to be located inside the treatment tank to compartmentalize the treatment system.
  - a. Equalization Zone/tank Wastewater will first be combined in an equalization zone/tank provided to allow for equalization (EQ) of peak flows prior to treatment in the Lyve system. Aeration will be provided in the equalization zone to allow for adequate mixing of the wastewater to occur.
  - b. pH adjustment A HACH pH analyzer/controller and a chemical dosing pump will be provided by Lyve for automatic adjusting for influent pH to remain between 6.8 and 7.2 pH units.
     Magnesium hydroxide will be used for pH adjustment in the wastewater stream.
  - c. MBBR Zone A zone will be provided in the treatment tank for biological treatment. The MBBR zone will contain plastic media which provides surface area for biomass to develop. Aeration is provided in this zone to promote biological growth and degradation of wastewater flows.
  - d. Activated Sludge Zone An activated sludge zone is provided in the treatment tank downstream of the MBBR zone to further treat process wastewater flows through activated sludge treatment. A coarse bubble diffuser is provided to allow for mixing and further degradation of wastewater flows.

e. Clarifier - Following the activated sludge zone, the wastewater will pass into a clarifier where clean effluent decants off the top and solids settle to the bottom. Clarified effluent will flow into a pump sump where it will be pumped out to the effluent storage pond. Solids that settle to the bottom of the clarifier will be pumped back to the selector zone. A measured amount

f. Sludge Digester Zone – A sludge digester zone will be provided in the main treatment tank for storage and digestion of wasted activated sludge from the clarifier. Periodic off-hauling or onsite pressing of the accumulated solids in the digester will be required unless an onsite sludge dewatering system is installed.

A control panel is and will continue to be provided for control of the blowers, pH monitoring and correction system, foam control, any influent pumps, effluent pump and other ancillary items. This system will include web based monitoring capabilities.

 Effluent Pumps –Duplex pumps will be capable of pumping treated effluent, with lead/lag and alternating pump capabilities, from the existing Lyve System out to the effluent pond.

of sludge is wasted to sludge digesters.

- 8) Flow measurement An inline flow measurement device will be provided to measure flows from the Lyve System to the effluent storage pond.
- 9) Effluent storage pond Effluent from the Lyve treatment system for Phase II will flow to an approximate 1.7 MGallon effluent storage pond (an existing irrigation pond that will be converted to an effluent storage pond).
- 10) Flow measurement An inline magnetic flow measurement device will be provided following the irrigation pump. This will allow for measurement of flows from the effluent storage pond to the surface disposal system.
- 11) Filtration/Disinfection Prior to surface disposal, effluent will go through a media filter and disinfected (via UV or Peroxyacetic acid) to meet Title 22, recycled water standards.
- 12) Effluent Surface Disposal –Final reuse (disposal) of effluent shall be accomplished by drip irrigation of a minimum of 10.0 acres (Phase II) of vineyard. The irrigation demand of the vineyard far exceeds the estimated annual wastewater volume (see Pond Water Balance in Enclosure C). To meet the additional irrigation demand the treated wastewater will be supplemented with irrigation water.

#### OTHER CONSIDERATIONS

#### ODOR CONTROL

There should be no noxious odors from a properly designed and operated treatment system. See Alternative Courses of Action for operation alternatives.

#### GROUND WATER CONTAMINATION

The nearest water well to the wastewater treatment and disposal system will be a minimum of 100 feet. No disposal of reclaimed wastewater will occur within 100 feet of any existing wells.

Irrigation/disposal of treated effluent is considered a beneficial use and is considered an effective means to

protect groundwater quality.

#### **PROTECTION**

Exposed wastewater treatment facilities should be posted with appropriate warning signs. The treatment areas will be protected to restrict access and potential damage to the system.

#### ALTERNATIVE COURSES OF ACTION

Although no operational difficulties are foreseen, the following additional courses of action would be available if necessary for the PW system:

- · Additional stages of treatment to increase effluent quality
- Increased use of irrigation/disposal area to increase discharge capacity
- Aeration in the effluent storage pond to improve effluent quality

The effluent storage pond will be sized for retention of wastewater effluent through the majority of the rainy season with minimal discharges to irrigation areas (if surface applied). Should there be a winter with more rainfall than the design condition; several operational procedures are available to compensate:

- · Additional water conservation at winery
- Light irrigation during periods between storms not exceeding the assimilative capacity of the soil
- · Increased irrigation during the months of planned irrigation
- Pumping and truck transfer of treated and diluted wastewater to an approved treatment plant or land disposal site

### **SOLID WASTES**

Solid wastes from the winery include primarily pomace, seeds, and stems. The estimated quantities of these wastes (at ultimate capacity) are as follows:

Phase II Annual Total = 
$$\frac{1 \text{ ton grapes}}{165 \text{ gal wine}} \times 660,000 \text{ gal wine} \times 35\% = 1,400 \text{ tons}$$

Based on a unit weight of 38 pounds per cubic foot, the annual volume of solids wastes would be:

1,400 tons 
$$\times \frac{2000 \text{ lb}}{1 \text{ ton}} = 2,800,000 \text{lb}$$
  
2,800,000 lbs  $\times \frac{1 \text{ ft}^3}{38 \text{ lb}} \times \frac{1 \text{ yd}^3}{27 \text{ ft}^3} = 2729 \text{ yd}^3$ 

These organic solids will be composted, spread on the vineyard, and disked in as a soil conditioner and supplemental nutrient source on a routine basis. This quantity of solids wastes is to be applied to the approximate onsite vineyard or will be hauled to an off-site composting location to reduce the application depth, if needed.

Contact: Gina Giacone gina@summit-sr.com (707) 636-9162



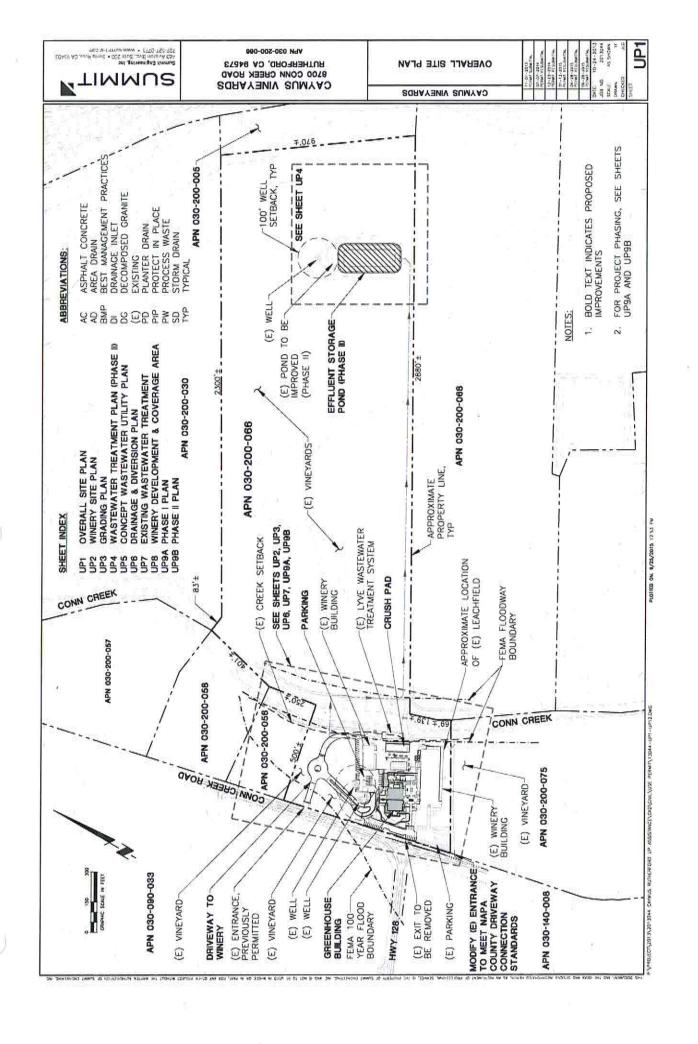
SUMMIT ENGINEERING, INC. 463 Aviation Blvd., Suite 200 Santa Rosa, CA 95403 707 527-0775 sfo@summit-sr.com

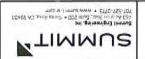
# **CAYMUS VINEYARDS**

# **ENCLOSURE A**

OVERALL SITE PLAN (UP1)
WASTEWATER TREATMENT PLAN (UP4)
CONCEPT WASTEWATER UTILITY PLAN (UP5)
EXISTING WASTEWATER TREATMENT (UP8)







APN 030-200-088

(E) WELL #4

100' WELL SETBACK, TYP

100,∓

Ŧ,Z9

(E) POND TO BEIMPROVED AND
CONVERTED TO
EFFLUENT
STORAGE POND
(PHASE II)

APN 030-200-066 CAYMUS VINEYARDS BYON CANDO, CAN CREEK ROAD RUTHERFORD, CA 94673

APN 030-200-005

₹,212.

PROPOSED EFFLUENT-STORAGE POND (PHASE II) (±1,7 MGAL)

APPROXIMATE PROPERTY UNE, TYP

WASTEWATER TREATMENT (II 38AH9) NAJ9

CAYMUS VINEYARDS

145'±

APN 030-200-068

UP4

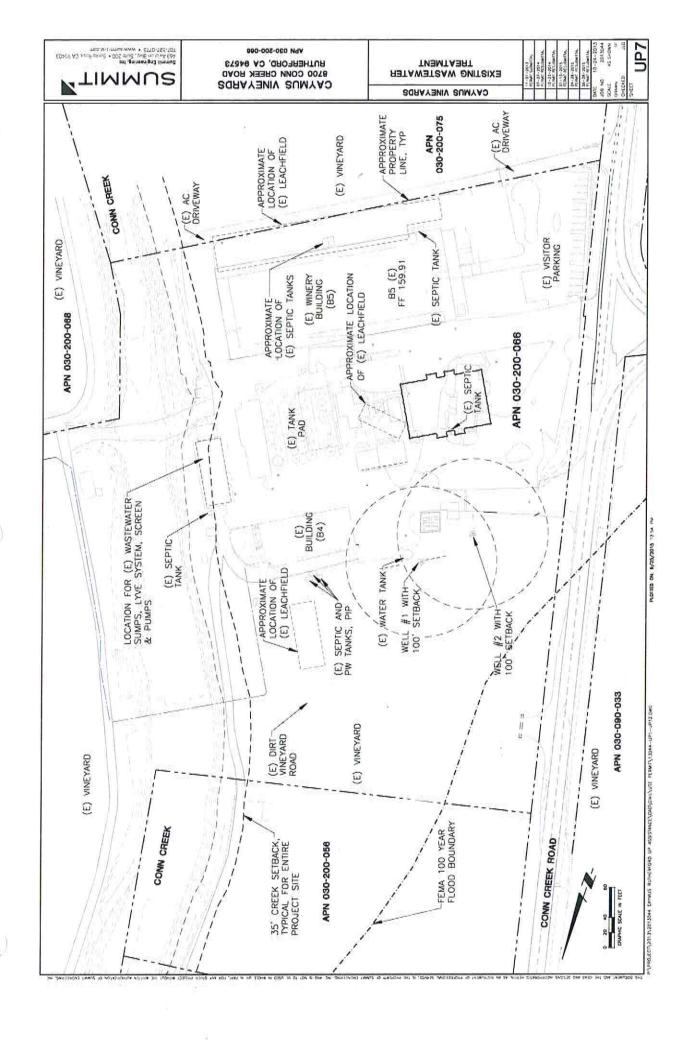
-(E) GROUND EARTHWORK: APPROXIMATE CUT: <500 CY APPROXIMATE FILL: 2,681 CY±

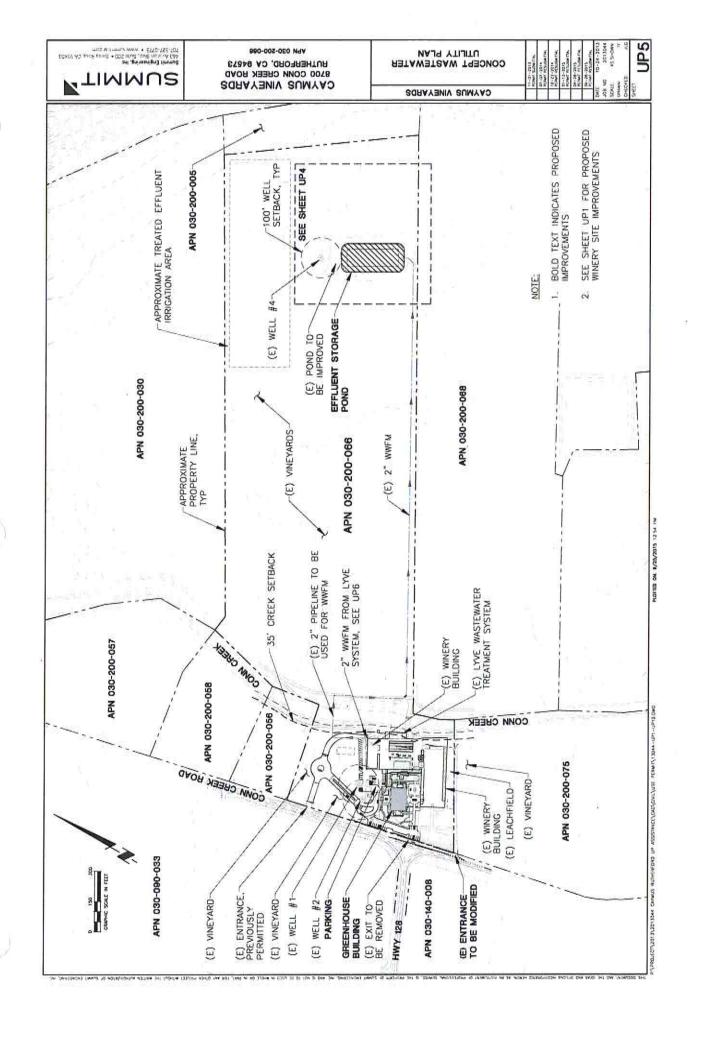
EFFLUENT STORAGE POND 313'± POND SECTION NEW POND BERM -3:1, TYP

62'±

100°±

(E) WELL #4-





# **CAYMUS VINEYARDS**

# **ENCLOSURE B**

PW POND EFFLUENT DISPERSAL WATER BALANCE (PHASE II)



#### SUMMIT ENGINEERING, INC. Consulting Civil Engineers

#### CAYMUS - RUTHERFORD Pond Water Balance - PHASE II

PROJECT NO. BY: CHK:

2013044 GG

# DESIGN CRITERIA

FULL PRODUCTION		ATT - DE TENTE ESITE
Annual Production	660,000 gal wine/yea	r
PW Generation Rate	4.0 gal PW/gal w	vine
Annual PW Flow	2,640,000 gal PW/year	
Months of Harvest	Aug-Oct	
Average Day PW Flow	7,240 gal PW/day	
Average Day Harvest PW Flow	11,500 gal PW/day	
Average Day Peak Harvest Month PW Flow	14,400 gal PW/day	
Average Day SS Flows	2,190 gal SS/day	
Peak SS Flows	3,690 gal SS/day	
Lyve System Inflow/Outflow	7,000 gal PW/day	
Effluent Storage Pond	1.706 Mgal	
Effluent Storage Pond HRT	112.3 days	(based on harvest flows)
Total HRT	112.3 days	<del></del>

**DESIGN PROCESS WASTEWATER FLOWS** 

Month	Monthly Percentage of Annual Flow <sup>a</sup> (%)	Monthly PW Flow (Mgal)	Approx Monthly SS Flow (Mgal)	Monthly PW & SS Flow (Mgal)	Average Daily Flow (gal/day)
August	10.5%	0.276	0.071	0.347	11,188
September	16.4%	0.433	0.069	0.502	16,722
October	12.9%	0.340	0.071	0.411	13,262
November	7.4%	0.196	0.069	0.264	8,812
December	6.4%	0.169	0.071	0.240	7,750
January	6.6%	0.173	0.071	0.244	7,877
February	7.2%	0.191	0.064	0.255	9,107
March	7.6%	0.201	0.071	0.272	8,784
April	6.8%	0.179	0.069	0.248	8,251
May	6.4%	0.170	0.071	0.241	7,779
June	5.6%	0.148	0.069	0.216	7,213
July	6.2%	0.164	0.071	0.234	7,563
Total	100%	2.640	0.835	3.475	

Monthly percentage of annual flow based on average of PW flow data from 11 wineries.

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**	Consu	T ENGINE Iting Civi	SUMMIT ENGINEERING, INC. Consulting Civil Engineers	ď	CAYMUS - RUTHERFORD Pond Water Balance - PHASE II Climate Data		PROJECT NO. BY: CHK:	2013044 GG 0
			7	٠				
		Average	Reference					
Month	Days	Days Temp <sup>a</sup> (F)	Evapotranspiration <sup>b</sup> (in)	Pan Evaporation <sup>c</sup> (in)	Lake Evaporation <sup>d</sup> (in)	Average Precipitation <sup>e</sup> (in)	Pan Evaporation <sup>c</sup> Lake Evaporation <sup>d</sup> Average Precipitation <sup>e</sup> 10-Year Precipitation <sup>(</sup> 100-Year Precipitation <sup>()</sup> (in) (in)	100-Year Precipitation <sup>†</sup> (in)
<b>August</b>	31	7.07	6.4	12.1	9.3	0.1	0.2	0.2
eptember	30	9'29	4,9	8.7	6.7	0.4	9.0	6.0
ctober	31	61.7	3.5	5.7	4.4	2.1	3.2	4.9
lovember	8	52.3	1.6	2.5	1.9	5.5	8.5	12.7
Secember	31	46.6	1.2	1.7	1.3	5.9	9.1	13.7
January	31	46	1.0	1.6	1.2	7.9	12.1	18.3
-ebruary	28	50.2	1.5	2.2	1.7	5.9	9.1	13.7
March	31	52.3	2.9	3.8	2.9	4.7	7.2	10.9
April	30	56.3	4.7	5.9	4.5	1.9	2.9	4.4
lay	31	62.4	5.8	0.6	6.9	0.4	9.0	6.0
June	9	89	6.9	11.0	8.5	0.1	0.2	0.2
uly	31	71.1	7.2	13.5	10.4	0.0	0.0	0.0
<b>Fotal</b>	365		47.7	77.7	59.8	34.9	53.6	80.9

<sup>a</sup> Average monthly temperature at St. Helena, 1961-1990. See http://www.worlddimate.com <sup>b</sup> Average monthly reference evaporation rates for Oakville (#77), 1989-2004 CIMIS, See http://www.cimis.water.ca.gov/cimis/data.jsp

Average monthly pan evaporation rates observed at Santa Rosa, Sonoma County, CA 1958-1970. Source James Goodridge.

d Pan evaporation rates adjusted by a factor of 0.77 to determine lake evaporation.

Average monthly rainfall observed at St. Helena, 1961-1990, See http://www.worldclimate.com

\* Average monthly rainfall adjusted by the ratio of 10-yr and 100-yr wet year return storm identified by Pearsons Log III Distribution (St. Helena)

SUMMIT ENGINEERING, INC. onsulting Civil EngineelVater Balance - PH	CAYMUS - RUTHERFORD Pond Water Balance - PHASE II Pond Worksheet	PROJECT NO. BY: CHK:	2013044 GG 0

Bottom Radius

Bottom Width Bottom Length Interior Side Slope (x:1) Length:Width

Depth	Length	Width	Radius	Surface Area	Total Volume
(#)	(ft)	(#)	(ft)	(ft²)	(Mgal)
0	240	85	15	20,208	0.000
Н	246	91	17	22,139	0.158
2	252	26	19	24,136	0.331
n	258	103	21	26,197	0.520
4	264	109	23	28,324	0.724
Ŋ	270	115	25	30,516	0.944
9	276	121	77	32,773	1.180
7	282	127	29	35,096	1.434
8	288	133	31	37,483	1.706
6	294	139	33	39,936	1.995
10	300	145	35	42,454	2.303

PROJECT NO. 2013044 BY: GG CHK: 0	
CAYMUS - RUTHERFORD PROJI Pond Water Balance - PHASE II BY; CHK:	
SUMMIT ENGINEERING, INC. ting Civil En Pond Water Balance - PHASE II	

			Lyve System								
Month	Tank Evaporation	>	10 Year	Volume Change	Divert	Surface	*neglect pr	*neglect precipitation and assume up to 7,000 gpd in & out	ssume up	to 7,000 gpd	in & out
		Inflow	Precipitation		Volume	Area		¥.			
	(Mgal)	(Mgal)	(Mgal)	(Mgal)	(Mgal)	(F)					
August	-0.0012	0.347	0.000020	0.346	0.346	208					
September	6000.0-	0.502	0.000080	0.501	0.501	208					
October	-0.0006	0.411	0.000419	0.411	0.411	208					
November	-0.0003	0,264	0.001096	0.265	0.265	208					
December	-0.0002	0.240	0.001176	0.241	0.241	208					
January	-0.0002	0.244	0.001574	0.246	0.246	208					
February	-0.0002	0.255	0.001176	0.256	0.256	208					
March	-0.0004	0.272	0.000937	0.273	0.273	208					
April	-0.0006	0.248	0.000379	0.247	0.247	208					
May	-0.0009	0.241	0.000080	0.240	0.240	208					
June	-0.0011	0.216	0.000020	0.215	0.215	208					
July	-0.0013	0.234	0.000000	0.233	0.233	208					
Total	-0.008	3,475	96900'0	3,474	3.474						
				Pond No.							
Month	Initial Volume	Pond	PW Inflow	10 Year	Volume	Total	Divert	Final Volume	Final	Volume	Surface
		Evaporation		Precipitation	Change	Volume	Volume		Pond	Check	Area
									Depth		
	(Mgal)	(Mgal)	(Mgal)	(Mgal)	(Mgal)	(Mgal)	(Mgal)	(Mgal)	( <del>L</del> )	(Mgal)	(ft <sup>2</sup> )
August	0.724	-0.165	0.346	0.004	0.185	0.909	0.300	0.609	3.4	0.000	28,324
September	609.0	-0.113	0.501	0.016	0.404	1.013	0.350	0.663	3.7	0.000	27,048
October	0.663	-0.076	0.411	0.085	0.420	1.083	0,350	0.733	4.0	0.000	27,686
November	0.733	-0.034	0.265	0.224	0.455	1.188	0.300	0.888	4.7	0.000	28,324
December	0.888	-0.025	0.241	0.240	0.456	1.345	0.200	1.145	5.8	0.000	29,859
January	1.145	-0.024	0.246	0.321	0,543	1.687	0.200	1.487	7.1	0.000	32,322
February	1.487	-0.037	0.256	0.240	0.459	1.946	0.241	1.706	8.0	0.241	35,334
March	1.706	-0.069	0.273	0.191	0.395	2.101	0.395	1.706	8.0	0.395	37,483
April	1,706	-0.106	0.247	0.077	0.219	1.925	0,219	1,706	8.0	0.219	37,483
May	1.706	-0.162	0.240	0.016	0.094	1.800	0.300	1.500	7.2	0.094	37,483
June	1.500	-0.188	0.215	0.004	0.031	1.531	0.413	1.118	-5.7	0.000	35,573
July	1.118	-0.208	0.233	0.000	0.025	1.144	0.420	0.724	4.0	0.000	32,096
Total		-1.206	3.474	1.420	3.688		3.688			0.949	

SUMMIT ENGINEERING, INC. ing Civil En Pond Water Balance - PHASE II	IG, INC. nce - PHASE II		CAYMUS - RUTHERFORD Pond Water Balance - PHASE II Irrigation & Effluent Application Rates	PROJECT NO. BY: CHK:	2013044 GG 0
Applied Irrigation Area	Vineyard Pasture	10:0	acres acres		

acres acres

Vineyard Pasture

Total Area Available for Imigation

Month	Reference ET	Pasture Crop Coefficient <sup>b</sup>	Vineyard Crop	Pasture ET	Vineyard ET	Precipitation*	Irrig	rrigation Nemand <sup>*</sup>	Operating Days	Percolatio Capacity	ation city <sup>h</sup>	Assim	Ssimilative Capacity <sup>1</sup>	Effluent	ent	Capacity
	(e)		Coefficient	120	í											
	(111)			(uı)	(m)	(III)	(III)	(Mgai)	<b>(b)</b>	(ii)	(Mgal)	(E)	(Mgal)	(Mgal)	(iii)	(Mgal)
August	6.4	6.0	0.5	5.8	2.9	0.2	2.7	0.746	31	446.40	121.294	449.1	122.040	0.300	1.10	121.74
September	4.9	6.0	0.3	4.4	1.3	9.0	0.7	0.177	28	432.00	117.381	432.7	117,558	0.350	1.29	117.21
October	3.5	6.0	0.1	3.2	0.2	3.2	0.0	0.000	16	230.40	62,603	230.4	62,603	0.350	1.29	62.25
November	1.6	0.8	0.0	13	0.0	8.5	0.0	0.000	14	201.60	54.778	201.6	54.778	0300	1.10	54.48
December	17	8.0	0.0	6.0	0.0	9.1	0.0	0.000	2	72.00	19,564	72.0	19,564	0.200	0.74	19.36
January	1.0	8.0	0.0	8.0	0.0	12.1	0.0	0.000	9	86.40	23.476	86.4	23,476	0.200	0.74	23.28
February	1.5	8.0	0.0	17	0.0	9.1	0.0	0.000	N	72.00	19.564	72.0	19.564	0.241	0.89	19.32
March	2.9	8.0	0.0	23	0.0	7.2	0.0	0.000	12	172.80	46,953	172.8	46,953	0.395	1.46	46.56
April	4.7	6.0	0.2	4.2	8.0	2.9	0.0	0.000	13	187.20	50.865	187.2	50.865	0.219	0.81	50.65
May	5.8	6.0	9.0	5.2	3.4	9.0	2.8	0.750	16	230.40	62,603	233.2	63,354	0.300	1.10	63.05
June	6.9	6.0	0.7	6.2	4. 9.	0.2	4.7	1.280	17	244.80	66,516	249.5	67.796	0.413	1.52	67.38
July	7.2	6.0	9.0	6.5	4.6	0.0	4.6	1.254	30	432.00	117.381	436.6	118,635	0.420	1.55	118.22
Total	47.7			42.1	18.0	53.6	15.5	4.2	195.0	2808.0	763.0	2823.5	767.3	37	126	762 SD

(a) Average monthly reference evapotranspiration rates, see Climate Data Worksheet.
 (b) Kc coefficients for pasture from Table 5-1, "Imgation with Reclaimed Municipal Wastewater-A Guidance Manual, 84-1 wr, SWRCB.
 (c) Kc coefficients for vineyards from Table 5-1, Imgation with Reclaimed Municipal Wastewater - A Guidance Manual, 84-1 wr, SWRCB.
 (c) Kc coefficients for vineyards from Table 5-1, Imgation with Reclaimed Municipal Wastewater - A Guidance Manual, 84-1 wr, SWRCB.
 (d) ET-ETO x Kc. A weighted value is determined on the basis of the available imgated acreage of vineyard and pasture.
 (e) Precipitation, 10-year ranifoll event, see Climate Data Worksheet.
 (f) Imgation Demand = ET-Precipitation, incles. A weighted value is determined on the basis of the available imgated acreage of vineyard and pasture.
 (g) Number of operating days per month based on estimated imgation days available based on 24-hr pre/post storm criteria for a 100-year return period. Summit Engineering, MBRID Capacity Study, April 1996.
 (h) Design percolation rate is a maximum of 0.58 inches per day for the number of operating days per month. Design percolation rate is a maximum of 0.58 inches per day for the number of operating days percolation rate is a maximum of 0.58 inches per day for the number of operating days percolation rate is a maximum of 0.58 inches per day for the number of operating days percolation rate is a maximum of 0.58 inches per day for the number of operating days percolation rate is a maximum of 0.58 inches per day for the number of operating days percolation rate is a maximum of 0.58 inches per day for the number of operating days percolation rate is a maximum of 0.58 inches per day for the number of operating days percolation rate is a maximum of 0.58 inches per day for the number of operating days percolation rate is a maximum of 0.58 inches per day for the number of operating days percolation rate i

adjusted by a 0.04 safety factor to account for typical slow rate land application design methodology.

(i) Assimilative capacity is the sum of irrigation demand and percolation applied.